



# CO<sub>2</sub> Emission Reduction Method Through Various Gas Turbine Fuel Applications

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## 1. Introduction

When discussing measures to prevent global warming, reducing carbon dioxide (CO<sub>2</sub>) emissions, which have the largest influence on the warming problem, is the most important issue. Measures against CO<sub>2</sub> emissions are largely divided into two fields, CO<sub>2</sub> emission reduction and CO<sub>2</sub> recovery. In addition, CO<sub>2</sub> emission reduction methods can be divided into two categories, improved efficiency of the energy conversion equipment and fuel conversion into hydrogen-rich fuel gases with less CO<sub>2</sub> emissions.

In power generating plants the improvement of thermal efficiency is already in progress through the introduction of gas turbine combined plants using high-performance gas turbines. For further progress in CO<sub>2</sub> emission reductions, the next generation of gas turbines with improved thermal efficiency must be developed.

On the other hand fuel conversion can be effectively addressed by modifying the design of combustors by use of existing gas turbine technology. Depending on the fuel properties after fuel conversion, a significant contribution to CO<sub>2</sub> emission reductions can be expected.

Regarding these needs, Mitsubishi Heavy Industries, Ltd. (MHI) has been continuously working for a long time on the development of hydrogen-rich gas fuel for gas turbines.

Currently, it already operates more than 10 commercial units. In this paper, we introduce the operational experience and design outline of hydrogen-rich gas firing and low-calorific gas firing gas turbines with relation to the various fuel applications.

## 2. Actual applications of various fuel gases

**Table 1** shows the types of fuel actually used in MHI gas turbines. There were 477 gas turbines as of December 2006. **Figure 1** shows the ranges of the calorific values of gas fuels.

Figure 1 shows the achievements obtained in the use of gas fuels with various ranges of calorific values, 2.5 MJ/m<sup>3</sup>N to 84 MJ/m<sup>3</sup>N. It should be noted that 11 low-calorific gas firing gas turbines of 4 MJ/m<sup>3</sup>N or less have been delivered to customers.

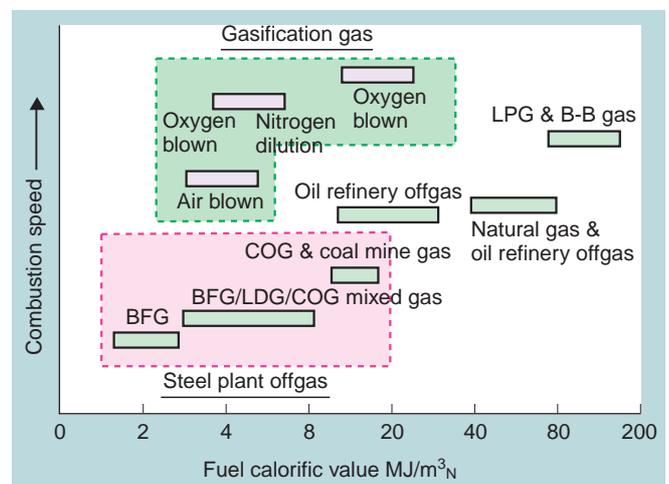
## 3. Development and evolution of gas turbines for hydrogen-rich gas

**Figure 2** shows the operational experience of our hydrogen-rich gas firing gas turbines whose hydrogen gas contents are 20 vol% or above. These gas turbines can be divided into three types based on their fuel source, the coke oven gas (COG) type, the oil refinery offgas type and the gasification gas type.

**Table 1** Types of fuel actually used in MHI gas turbines

Fuel	Number of units
1. Single fuel	
(1) Natural gas or LNG	187
(2) Oil refinery offgas/LPG	19
(3) Steel plant offgas	25
(4) Diesel oil	63
(5) Others	1
2. Dual fuels	
(1) Natural gas/diesel oil	157
(2) Natural gas/heavy oil	6
(3) Oil refinery offgas/diesel oil	7
(4) LPG/diesel oil	7
(5) Steel plant offgass/diesel oil	3
(6) Coal gasification gas/diesel oil	1
(7) VR gasification gas/diesel oil	1
Total	477

(As of December 2006)



**Fig. 1** Actual experience of fuel gas

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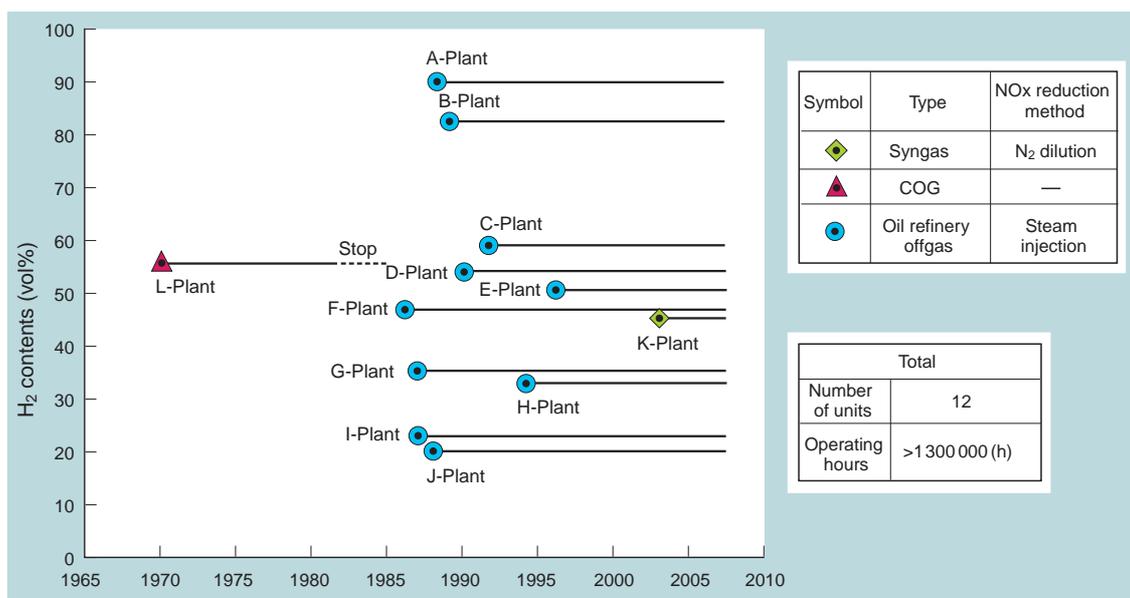


Fig. 2 Operational experience of hydrogen-rich gas (20 vol% or above) firing gas turbine

Table 2 Main specifications of 431MW VR gasification gas firing combined cycle plant

	Gross plant output (MW)	431
	Net plant output (MW)	342
	Fuel main/auxiliary	VR gasification gas/kerosene
Gas turbine	Type	Simple open cycle, single shaft M701F
	Output (MW)	301
	Rotation speed (min <sup>-1</sup> )	3 000
Steam turbine	Type	Single cylinder, down exhaust condensing reheat type
	Output (MW)	130
	Rotation speed (min <sup>-1</sup> )	3 000
	Steam conditions	Steam turbine inlet
	Main steam	9.8 MPaG × 538°C
Reheat steam	2.9 MPaG × 538°C	
Medium pressure steam	0.7 MPaG × 313°C	
Power generator	Type	AC three phase/synchronous, H <sub>2</sub> cooling type
	Capacity (kVA)	479 390
	Voltage (kV)	23
	Rotation speed (min <sup>-1</sup> )	3 000
Heat recovery steam generator	Type	Reheat triple pressure vertical natural circulation type

Ambient temperature: 15°C, atmospheric pressure: 0.1013MPa, relative humidity: 60%

The first hydrogen-rich gas firing gas turbine started commercial operation in 1970 as a 30 MW gas turbine using COG as fuel and with the inlet temperature of 700°C. This COG is a by-product gas produced in coal chemical plants whose hydrogen content exceeds 50 vol%. In addition to its high hydrogen content, as COG contains impurities, various measures were taken for the gas turbine combustor and the fuel treatment and supply systems.

Since the beginning of the 1980s and especially after the oil crises, the industry has become very aware of energy saving and the need for the petrochemical industry to use hydrogen-rich gas from oil refinery processes as gas turbine fuel has increased. Along with this, due to the need to supply high-temperature, high-pressure steam from gas turbine exhaust gas by using a heat recovery steam generator, a 1,250°C class gas turbine was developed which was a great achievement at that time.

Flashback in the gas turbine combustor was one of the important issues when hydrogen-rich gas was used as fuel for high-temperature gas turbines and it was successfully overcome by adoption of a fuel nozzle configuration.

Ten hydrogen-rich gas (oil refinery offgas) firing gas turbines were delivered and are still operating successfully today.

Based on the operational experience of these units and the operational experience of the low-calorific gas firing gas turbines described in Section 4, we delivered a hydrogen-rich gas (VR gasification gas) firing gas turbine combined plant with a capacity of 431 MW, the world's largest gas turbine, to Negishi Refinery of Nippon Oil Refining Company in 2003.

Table 2 and Fig. 3 show the main specifications and an outline of this plant. Here, NOx control was the major issue to be addressed for the fuel of this plant.

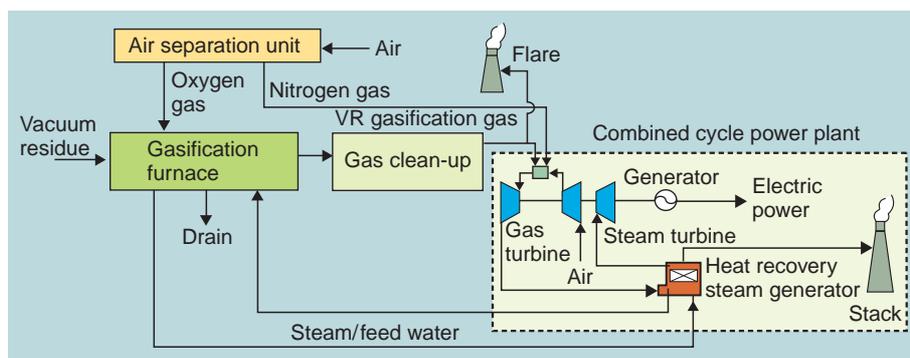


Fig. 3 Outline of 431 MW VR gasification gas firing combined plant

The VR gasification gas produced in a gasification furnace has a very high adiabatic flame temperature and will generate a high NO<sub>x</sub> level if burned without NO<sub>x</sub> reduction. Therefore, in this plant, nitrogen supplied from the air separation unit is mixed with VR gasification gas and this mixed gas is used as the gas turbine fuel. This mixed gas, compared with liquefied natural gas (LNG), has a low calorific value and adiabatic flame temperature, which contributes to reducing NO<sub>x</sub> emissions. Because of its high hydrogen content, it has a higher combustion speed and wider flammability ranges. Because of these fuel characteristics, the NO<sub>x</sub> level at the gas turbine outlet can be reduced to a level as low as that for a premixed combustor of natural gas even if a diffusion combustor is used. Thus, this plant has adopted the use of a diffusion combustor which provides stable combustion even with changes in the fuel properties.

Also, in this plant, as the gas turbine needs to be started in advance by kerosene fuel before the gasification furnace is started, the combustor has been designed to support the dual fuel firing of gas and oil.

#### 4. Development and evolution of gas turbines for low-calorific gas

The Japan's first BFG firing gas turbine (output: 850 kW) was delivered to Yawata Iron & Steel Co. (now Nippon Steel Corporation) in 1958 and the MW171 gas turbine (output: 15 MW) was delivered to Sumitomo Metal Industries, Ltd. Wakayama Works. Subsequently, the thermal efficiency of the gas turbine itself has been improved by increasing the turbine inlet temperature and by improving the efficiency of each component. Further, the increased gas turbine exhaust gas temperature has contributed to improving the energy recovery efficiency of the heat recovery steam generator.

In the evolution described above, a M151 gas turbine (with a turbine inlet temperature of 1,000°C or above) plant was delivered to Nippon Steel Corporation, Kamaishi Works in 1982, and a 145 MW class gas turbine combined cycle plant was delivered to JFE Steel Co., Ltd., East Japan Works (Chiba) in 1987.

Based on our operational experience of this large-capacity combined cycle plant, we delivered a plant of the

same size equipped with a DA type gas turbine which has a 100°C higher turbine inlet temperature than D type to Kurashiki Power Plant and Fukuyama Power Plant of Setouchi Joint Thermal Power Co., Ltd. in 1994 and 1995. In addition, through the integration of these technologies, with Kimitsu Power Plant of Kimitsu Corporative Thermal Power Company, Inc., we delivered a high-efficiency, large-capacity, BFG firing, combined cycle plant which, as the world's first F type gas turbine, realizing a turbine inlet temperature of 1,300°C, the highest temperature of all BFG firing gas turbines. Along with the recent rapid growth of the iron industry in China and South Korea, the number of BFG firing gas turbines delivered has been increasing. **Table 3** shows the delivery record.

#### 5. Effect of CO<sub>2</sub> emission reduction in BFG firing combined plant

Carbon dioxide (CO<sub>2</sub>) emissions are interrelated with the BFG/COG quantity of the by-product gas from iron works. As the BFG/COG quantity is determined by the crude steel production, CO<sub>2</sub> reductions need to be evaluated not only in terms of the power plants using these by-product gases but also by including the surrounding equipment. The following shows an evaluation plan:

In developing countries, BFG is not currently used for power plants but is flared into the atmosphere. A comparison of this with the situation after the introduction of gas turbine combined plants (GTCC) is shown in **Fig. 4**.

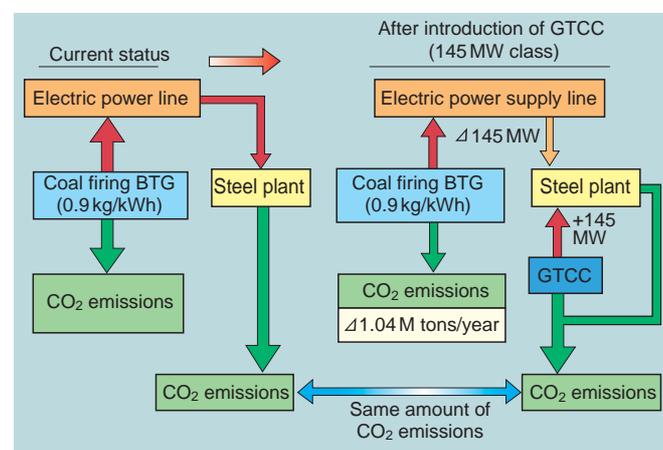


Fig. 4 Schematic diagram of CO<sub>2</sub> reduction in a steel plant

**Table 3 Delivery record of low calorific gas firing gas turbines**

Client	Plant	Start-up date	Type	Plant output	Fuel		Combustion unit
					Main	Auxiliary	
Yawata Iron & Steel Co. (Yawata)	Air blower	1958	-	0.85MW	BFG (3.2MJ/m <sup>3</sup> N)	-	Single can
Yawata Iron & Steel Co. (Yawata)	Air blower	1964	-	4MW	BFG (3.2MJ/m <sup>3</sup> N)	-	Single can
Sumitomo Metal Industries, Ltd. (Wakayama)	Cogeneration (WHB, G-M, BLOWER)	1965	MW171	15MW	BFG (3.1MJ/m <sup>3</sup> N)	-	Single can
Shikoku Electric Power Co., Inc. (Sakaide)	Combined cycle	1970	MW301	225MW	COG (18.8MJ/m <sup>3</sup> N)	-	Multi can
Mistubishi Coal Mining Co. (Minami Oyubari)	Cogeneration	1970	MW101	9MW	Coal mine gas (20MJ/m <sup>3</sup> N)	Oil	Multi can
Nippon Steel Corporation (Kamaishi/Oita)	Combined cycle (Utilization of an existing ST)	1982	M151	16MW	BFG (2.8MJ/m <sup>3</sup> N)	-	Single can
JFE Steel Corporation (Chiba)	Combined cycle (single shaft type)	1987	M701	149MW	BFG/COG (4.2MJ/m <sup>3</sup> N)	-	Multi can
Mitsubishi Gas Chemical Company, Inc. (Mizushima)	Cogeneration	1988	MF111	16MW	BFG/COG (10MJ/m <sup>3</sup> N)	Oil	Multi can
Nisshin Steel Co., Ltd. (Kure)	Combined cycle (Utilization of an existing ST)	1989	M251	32MW	BFG (2.9MJ/m <sup>3</sup> N)	-	Multi can
Nippon Steel Corporation (Hirohata)	Combined cycle (Utilization of an existing ST)	1989	M251	30MW	LDG (7.6MJ/m <sup>3</sup> N)	Oil	Multi can
Nakayama Steel Works, Ltd. (Funamachi)	Combined cycle (single shaft type)	1991	M151	37MW	BFG/LDG (4.2MJ/m <sup>3</sup> N)	-	Multi can
Setouchi Joint Thermal Power Co., Ltd. (Kurashiki)	Combined cycle (single shaft type)	1994	M501DA	149MW	BFG/COG (4.0MJ/m <sup>3</sup> N)	-	Multi can
Setouchi Joint Thermal Power Co., Ltd. (Fukuyama)	Combined cycle (single shaft type)	1995	M501DA	149MW	BFG/COG (4.0MJ/m <sup>3</sup> N)	-	Multi can
NUON (Netherlands)	Combined cycle (single shaft type)	1997	M701	145MW	BFG/COG (4.2MJ/m <sup>3</sup> N)	-	Multi can
Nippon Steel Corporation (Oita)	Combined cycle	2001	M251	67MW	BFG (2.9MJ/m <sup>3</sup> N)	-	Multi can
Nippon Oil Refining Co. (Negishi)	Combined cycle (single shaft type)	2003	M701F	431MW	Syngas+N <sub>2</sub> (5.9MJ/m <sup>3</sup> N)	Oil	Multi can
Kimitsu Cooperative Thermal Power Co. (Kimitsu)	Combined cycle (single shaft type)	2004	M701F	300MW	BFG/COG (4.4MJ/m <sup>3</sup> N)	-	Multi can
Zhangjiagang Hongchang Plate Co. (China)	Combined cycle	2006	M251	30MW x 4	BFG (3.1MJ/m <sup>3</sup> N)	-	Multi can
Anshan Steel Co. (China)	Combined cycle (single shaft type)	2007	M701F	300MW	BFG/COG (4.4MJ/m <sup>3</sup> N)	-	Multi can
Handan Steel Co. (China)	Combined cycle	2006	M251	30MW x 2	BFG (3.1MJ/m <sup>3</sup> N)	-	Multi can
Maanshan Iron & Steel Co. (China)	Combined cycle (single shaft type)	2007	M701DA	153MW	BFG/COG (4.4MJ/m <sup>3</sup> N)	-	Multi can
POSCO (South Korea)	Combined cycle (single shaft type)	2007	M501DA	146MW	FOG (5.7MJ/m <sup>3</sup> N)	-	Multi can
Clean Coal Power R&D Co., Ltd. (Nakoso)	Combined cycle (single shaft type)	2007	M701DA	250MW	Syngas (4.2MJ/m <sup>3</sup> N)	Oil	Multi can
Lianyuan Steel Co. (China)	Combined cycle	2007	M251	30MW	BFG (3.1MJ/m <sup>3</sup> N)	-	Multi can
Baotou Steel Co. (China)	Combined cycle (single shaft type)	2008	M701DA	138MW x 2	BFG/COG (4.4MJ/m <sup>3</sup> N)	-	Multi can
IUD (Ukraine)	Combined cycle (single shaft type)	2009	M701DA	151MW x 2	BFG/COG (4.4MJ/m <sup>3</sup> N)	-	Multi can

When 145 MW of power is generated by a BFG firing GTCC, 145 MW being generated in a coal firing steam power plant (BTG) can be reduced. If the annual generating duration of a coal firing BTG is assumed to be 8,000 hours, the CO<sub>2</sub> emissions from this coal firing BTG, which amounts to 1,040,000 tons/year of CO<sub>2</sub>, can be reduced.

When compared to a newly established BTG, a GTCC will yield a further reduction of about 200,000 tons/year as shown in Fig. 5.

As described above, from the viewpoints of improved plant efficiency and the emission control of CO<sub>2</sub> through the effective use of BFG, the advantages of the gas turbine combined cycle plant can be confirmed.

## 6. Conclusion

Power generation plants based on hydrogen-rich gas firing gas turbines and low-calorific gas firing gas turbines (mainly BFG) have already accumulated extensive operational experience and the construction of many more power generation plants are scheduled both overseas and in Japan in the near future. The development of this technology, we believe, can greatly contribute to society by responding to demands for the effective use of energy and global environmental measures. We are fully determined to continue our efforts in technological development and continue working as pioneers in this field.

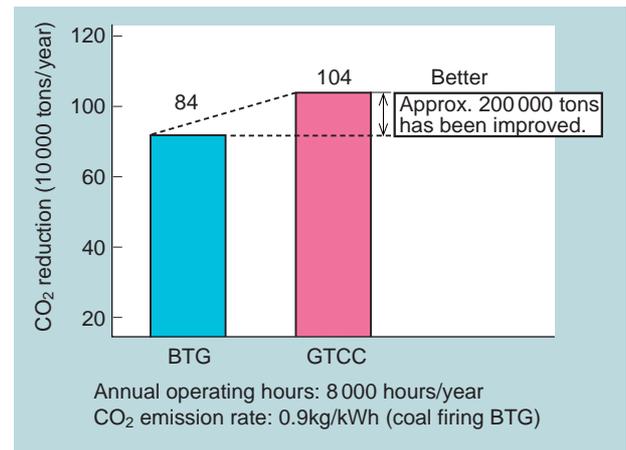


Fig. 5 Comparison of CO<sub>2</sub> reductions

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